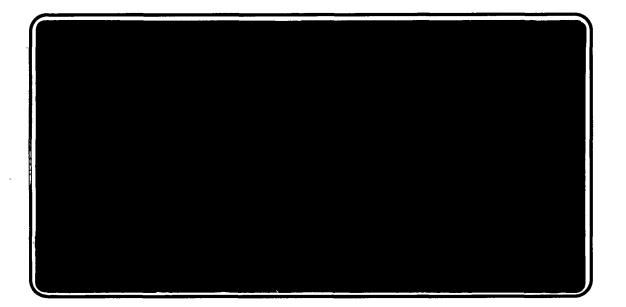
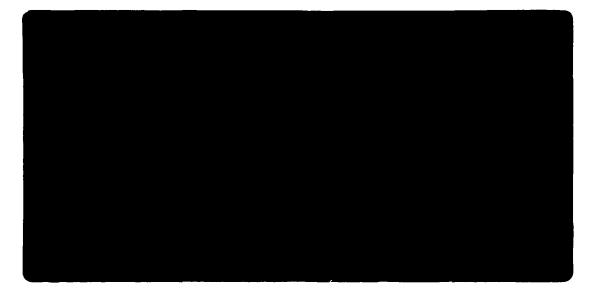
ENTERED JUN 0 4 1992



Institute of Paper Science and Technology Atlanta, Georgia

IPST TECHNICAL PAPER SERIES





NUMBER 443

THERMAL COATING DEVELOPMENT FOR IMPULSE DRYING

W.J. LENLING, M.F. SMITH, AND D.I. ORLOFF

MAY 1992

1

Thermal Coating Development for Impulse Drying

W.J. Lenling, M.F. Smith, and D.I. Orloff

To be published in the Proceedings of the 1992 International Thermal Spray Conference (ITSC '92)

Copyright[©] 1992 by The Institute of Paper Science and Technology

For Members Only

NOTICE & DISCLAIMER

The Institute of Paper Science and Technology (IPST) has provided a high standard of professional service and has put forth its best efforts within the time and funds available for this project. The information and conclusions are advisory and are intended only for internal use by any company who may receive this report. Each company must decide for itself the best approach to solving any problems it may have and how, or whether, this reported information should be considered in its approach.

IPST does not recommend particular products, procedures, materials, or service. These are included only in the interest of completeness within a laboratory context and budgetary constraint. Actual products, procedures, materials, and services used may differ and are peculiar to the operations of each company.

In no event shall IPST or its employees and agents have any obligation or liability for damages including, but not limited to, consequential damages arising out of or in connection with any company's use of or inability to use the reported information. IPST provides no warranty or guaranty of results.

To be published in the Proceedings of the 1992 International Thermal Spray Conference (ITSC'92), Orlando, FL, June 1-5, 1992 - - available from ASM International, Materials Park, OH 44073

Thermal Coating Development for Impulse Drying

William J. Lenling

Thermal Spray Technologies, Watertown, WI 53094 USA Phone (414) 261-0131, Fax (414) 261-4549

Mark F. Smith

Sandia National Laboratories,^{*} Albuquerque, NM 87185 USA Phone (505) 845-3256, Fax (505) 845-3130

David L Orloff

Institute of Paper Science and Technology,[†] Atlanta, GA 30318 USA Phone (404) 853-9781, Fax (404) 853-9510

Abstract

A special plasma sprayed coating has been developed for the heated surface of rolls used in a new energy-efficient paper drying process, known as "Impulse Drying," which could save the U.S. paper industry an estimated \$800 million annually in reduced energy costs. Because impulse drying rolls operate at substantially higher surface temperatures than conventional drying rolls, the thermal properties of the roll surface must be carefully tailored to control energy transfer to the paper, and thus prevent sheet delamination or other undesirable effects. To meet this requirement, a special plasma sprayed thermal barrier coating has been developed to control thermal mass, heat transfer, and steam infiltration. A coated test platen significantly outperformed a comparable uncoated steel platen in preliminary experiments with a heavy-weight paper grade on a laboratory-scale impulse drying simulator. Based on these results, the coating was then tested on the roll of a pilot-scale impulse dryer. In comparison to conventional wet-pressing, linerboard that was impulse dried with the coated test roll showed marked improvements in water removal as well as improved physical properties, such as density and specific elastic modulus. The successful prototype coating design has three plasma sprayed layers that are deposited sequentially: 1) a nickel alloy bond coat; 2) a thick, 17% porous, zirconia thermal barrier; and 3) a thin, 5-7% porous, zirconia top coat.

THE PULP AND PAPER INDUSTRY is one of the largest industrial consumers of energy in the United Sates [1-3]. Based on an average of 35 MJ per kg (30 million BTU's per ton) of paper produced and an annual production of 7×10^{10} kg (76 million tons) of paper, this industry consumes an estimated 2.4×10^{18} J (2.3 Quads) of energy annually. Drying is the largest single use of energy in the papermaking process and accounts for about one quarter of the total energy consumption. Therefore, even a modest improvement in drying efficiency can yield substantial energy and cost savings.

In conventional wet-pressing and evaporative drying processes, a great deal of energy is required in order to heat and vaporize water. The impulse drying process takes advantage of a different water removal mechanism. In this process, a steam pulse propagates through the paper and expels much of the water in liquid form, thus saving a significant amount of energy that would normally be required to heat and vaporize that water. In typical impulse drying, wet paper is brought into contact with a press roll that has been heated to a temperature of 473 to 673 K (200 to 400 °C), and a peak pressure of 3 to 6 MPa (435 to 870 psi) is applied for 20 to 40 milliseconds as the paper passes through the nip (i.e., the high-pressure "pinch" region) of a drying press. Under these conditions, water at or near the interface between the sheet and the heated roll surface flashes to steam. This steam layer grows and propagates through the sheet, displacing liquid water into a receiver, typically a press felt, that is in direct contact with the sheet on the side opposite to the heated roll. It is estimated that wide-scale implementation of impulse drying could reduce paper drying costs in the U.S by at least 10%, a potential savings of roughly \$800 million annually.

Although the basic principles and potential advantages of impulse drying have been known for some time, prior research [4-7] has shown that delamination of paper sheet subjected to impulse drying is a serious problem that must be solved before this process can be commercialized. The delamination problem was most apparent when drying heavy-weight paper grades, such as linerboard. This was extremely unfortunate, because these grades have the greatest potential for significant energy savings.

Researchers at the Institute of Paper Science and Technology (IPST) hypothesized that delamination is caused by the transfer of excess energy into the paper, with the result that water in the inner part of the sheet becomes superheated. Then, as the sheet leaves the nip and the applied pressure is rapidly released, the superheated water within the sheet flashes to steam, causing the sheet to delaminate. In order to test this hypothesis, IPST performed tests with a laboratory-scale impulse drying simulator (Fig. 1) using different materials to alter the heat input to the paper sheet [8-10]. Platens for the impulse drying simulator were made from the following materials: steel, aluminum, porous sintered stainless

This work was performed in part at Sandia National Laboratories, operated for the U.S. Department of Energy under contract number DE-AC04-76DP00789.

[†] Work at the Institute was sponsored by the member companies of the Institute of Paper Science and Technology and by the U.S. Department of Energy under contract number FG02-85CE40738.

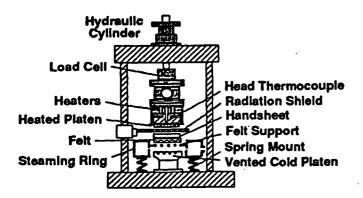


Fig. 1 - Electro-hydraulic press used to simulate wet pressing and impulse drying.

steel (two different densities), and a low-thermal-mass machinable ceramic. The steel and aluminum resulted in different heat fluxes to the paper sheet, but the effect on delamination was negligible. The porous stainless steel platens suppressed delamination, but venting of steam into the porous platen surface reduced the intensity of the steam pulse in the sheet, thus greatly decreasing the expulsion of liquid water into the felt and reducing drying efficiency. The machinable ceramic provided good water removal, and it also reduced delamination by limiting the transfer of excess energy to the sheet. Unfortunately, commercial drying rolls are quite large, typically on the order of 1.2 m (4 ft) in diameter by 6.1 m (20 ft) long, and it is not practical to produce such a roll from a monolithic ceramic material.

In view of the success of the ceramic platen tests at IPST, it was proposed that a plasma sprayed ceramic coating on a conventional steel roll might provide a practical way to achieve the desired thermal properties and performance. With funding from the U.S. Department of Energy, a joint research program to produce and test plasma sprayed coatings for possible use on impulse drying rolls was initiated by the Institute of Paper Science and Technology, Thermal Spray Technologies (TST), and Sandia National Laboratories.

Materials Selection

In order to minimize energy transfer to the paper sheet, the coating material should have a low thermal conductivity and a low heat capacity. Four common oxides, Al_2O_3 , TiO_2 , ZrO_2 , and SiO_2 , were selected for initial consideration on the basis of published thermal properties [11]. For a given coating material, the level of porosity in the coating also has a strong influence on the bulk thermal conductivity and bulk heat capacity of the coating. The heat flux into the paper sheet was calculated for each of the four candidate materials with various levels of porosity, and the results were normalized to the heat flux that would occur with a conventional, uncoated steel roll. The computed results in Fig. 2 show that the heat flux into the paper decreases in a nearly linear relationship as the porosity increases for each of the four candidate materials. (Additional details concerning these calculations are presented in [10].)

Based on the results in Fig. 2, zirconia or silica would be the best choices to minimize the heat flux to the paper sheet. Zirconia was selected for further development for several reasons. Fine silica powder is a potential health hazard, and zirconia is much easier to plasma spray than silica. Also, since plasma sprayed zirconia thermal barriers are used extensively for aircraft engines and other commercial applications, many different types of highquality zirconia powders custom-tailored for plasma spraying are commercially available. For this initial proof-of-concept study, an

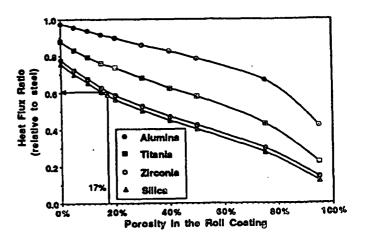


Fig. 2 - Calculated heat flux into a paper sheet as a function of the porosity in the candidate coating material. These results are based on an initial roll temperature of 573 K (300 °C), and they have been normalized to the heat flux from an uncoated steel roll.

arc-fused/spray-dried, partially stabilized zirconia (PSZ) containing 8.0 wt. % yttria, 1.7 wt. % hafnia, and 0.4 wt. % silica, was selected. This material was chosen primarily because research has shown that arc-fused/spray-dried powders tend to produce more porous coatings than hollow spherical powder (HOSP) or fused and crushed materials [12]. Also, this particular spray powder, Zircoa Zirspra[™] 9204, has previously performed very well in other thermal barrier applications at Sandia and at TST. The particle size range of the zirconia powder was -100 to +44 microns.

Thermal Properties of Sprayed Zirconia

In order to provide more accurate thermal property data for analytical modeling of the impulse drying process, a contract was placed with Properties Research Laboratory of West Lafayette, Indiana, to measure the specific heat and thermal diffusivity of the plasma sprayed zirconia as a function of temperature. These measurements were repeated for a series of sprayed samples with porosities ranging from 5% to nearly 20% by volume. The resulting data were used to predict the specific heat and thermal diffusivity for a theoretical full-density (0% porosity) plasma sprayed material. Plots of the predicted properties for the fulldensity sprayed material as a function of temperature are shown in Fig. 3.

A parameter called the "thermal mass," defined as the ratio of the thermal conductivity to the square root of the thermal diffusivity, is useful in considering potential surfacing materials for impulse drying. Thermal mass (K) can also be expressed as follows:

$$K = \left[\rho C_{p} \sqrt{\alpha}\right]_{\text{solid}} \left\{\frac{1 - V}{1 + C V}\right\}^{1/2}$$

where $\rho = \text{density}$, $C_{p=}$ specific heat, and $\alpha = \text{thermal diffusivity}$ of the solid ceramic; $V = \text{the volume fraction of pores in the$ sprayed coating; and <math>C' = 8.52 is a correlation coefficient determined from a best fit to measured data. As shown in Fig. 4, the thermal mass of a plasma sprayed PSZ coating decreases significantly with increasing porosity, but it is relatively insensitive to operating temperature up to at least 800 K (527 °C). In general, the ideal coating should have the lowest practical K value, which is consistent with the earlier statement that high porosity is desirable for the impulse drying roll coating.

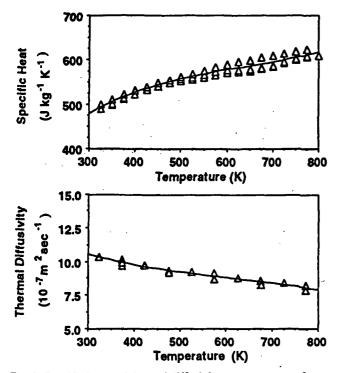


Fig. 3 -Specific heat and thermal diffusivity vs. temperature for a theoretical, full-density, plasma sprayed 8 wt.% yttria - 1.7 wt.% hafnia partially stabilized zirconia.

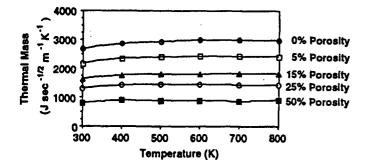


Fig. 4 - Thermal mass of 8% yttria -1 .7% hafnia PSZ as a function of porosity and temperature.

Coating Design for Impulse Drying Tests

A porous zirconia coating sprayed directly onto a steel platen or roll would meet the basic requirement for a low thermal mass coating. However, additional factors, such as adhesion of the coating to the substrate and possible venting of steam into the porous coating, must be considered in actual practice. For these reasons, the test coating actually consisted of three layers that were plasma sprayed sequentially onto the test hardware: 1) a metal alloy bond coat; 2) a thick, porous, PSZ thermal barrier, and 3) a thin, relatively dense, PSZ top coat.

Bond Coating. Among the many commercially available bond coating materials a Ni - 6.5 Al - 6.0 Mo (wt.%) alloy with a -105 to + 44 micron particle size distribution was selected for the impulse drying application. This powder was purchased from Anval of Rutherford, New Jersey. Prior experience has shown that this bond coating provides good ASTM tensile adhesion of ceramics to metals, typically 20 to 35 MPa (3 to 5 ksi), and that it can be sprayed at relatively high deposition rates, on the order of 0.08 mm (0.003 in) per pass. Although several other bond coatings would probably afford acceptable adhesion, a high deposition rate is particularly attractive for the impulse drying application due to the exceptionally large surface area to be coated on an actual commercial drying roll.

Surfaces of the test samples were cleaned and degreased with 1,1,1 trichloroethane and then grit blasted with 36 mesh aluminum oxide at a blasting pressure of 275 kPa (40 psi) before a final trichloroethane rinse. The bond coating was then applied to a thickness of 0.08 - 0.13 mm (0.003 - 0.005 in) using the plasma spray parameters shown in Table I.

Porous Zirconia. Although high porosity in the sprayed coating is desirable for impulse drying, there are practical limits to the porosity that can be produced in a sprayed coating for this application. The upper limit of porosity that could be reproducibly achieved with a reasonable deposition efficiency was 17%, as determined quantitative image analysis of the relative areas of solid ceramic and pores in polished metallographic sections. It is noteworthy that the procedure used for metallographic preparation of brittle coating materials, such as porous ceramics, can strongly influence the apparent porosity in a polished metallographic mount. An investigation of this problem and a detailed description of the procedure used to prepare the metallographic samples for this study have been presented in a prior publication [13].

From Fig. 2, a 17% porous zirconia coating should ideally result in a heat flux to the paper sheet that is approximately 60% of the heat flux from an uncoated steel roll operated at 573 K (300 °C). Therefore, even though a further increase in porosity might be desirable, the 17% porous coating still provides a very

Process	Ni-Al-Mo	17% Porous	5 - 7% Porous
Parameter	Bond Coat	Zirconia	Zirconia
Anode Type	2083-119MI	2083-119MI	2083-165
Cathode Type	1083A-120	1083A-120	1083A-129
Gas Injector	1083A-121	1083A-121	2083-130
Arc Gas & Flow	Argon @ 47 ltr/min	Argon @47 ltr/min	Argon @ 47 ltr/min
Aux Gas & Flow	Helium @ 20.5 ltr/min	Helium @ 20.5 ltr/min	Helium @ 20.5 ltr/min
Arc Current	800 amps	950 amps	950 amps
Arc Voltage	37 volts	38 volts	37 volts
Carrier Gas	Argon @ 5 ltr/min	Argon @ 5 hr/min	Argon @ 5 ltr/min
Powder Feed	39.9 g/min	44.5 g/min	44.5 g/min
Spray Distance	10 cm	10 cm	9 cm
Traverse Rate	51 cm/sec	51 cm/sec	51 cm/sec

Table I: Plasma Spray Parameters*

* All coatings were deposited with a Miller Thermal Technologies model SG-100 plasma gun.

significant potential reduction in energy transfer to the paper sheet. Using the spray parameters summarized in Table I, a 0.38 mm (0.015 in) thick layer of 17% porous zirconia was deposited over the Ni-Al-Mo bond coating on the steel test hardware.

Top Cost. The results described earlier for impulse drying simulator tests with porous stainless steel platens suggest that excessive escape of steam into a porous coating might reduce the intensity of the steam pulse propagating through the sheet, thus decreasing the expulsion of liquid from the sheet into the felt. In order to minimize steam infiltration into the coating, a thin, dense top coat was applied over the high-porosity zirconia. Initially two different top coating materials were tried. One was the same zirconia spray powder that was used for the 17% porous zirconia layer, but the plasma spray parameters were adjusted (Table I) to reduce the porosity in the deposited zirconia down to approximately 5% to 7%. The dense zirconia top coat was kept relatively thin, with a final thickness of approximately 0.05 mm (0.002 in) after the coating surface was diamond ground to a 20 µm rms finish. Therefore, the overall bulk properties of the porous and dense layers of sprayed zirconia were still dominated by the much thicker layer of 17% porous material. Microstructures representative of the nickel alloy bond coat, the 17% porous zirconia, and the 5 - 7 % zirconia top coat are shown in Fig. 5.

As an alternative to the dense zirconia top coat, a few experiments were also conducted with a thin layer of copper plasma sprayed over the porous zirconia. Because copper has a higher thermal conductivity and heat capacity than zirconia, the thin copper coat was tried in order to explore the effects of a more intense initial heat pulse. The copper top coat was kept as thin as possible, approximately 0.025 to 0.050 mm (0.001 to 0.002 in) after finish grinding of the sprayed surface, in an effort to limit its thermal mass contribution. Nevertheless, the copper-coated test platen produced significant sheet delamination in laboratory-scale impulse drying tests. This demonstrates that it is extremely important to maintain a low thermal mass in the coating.

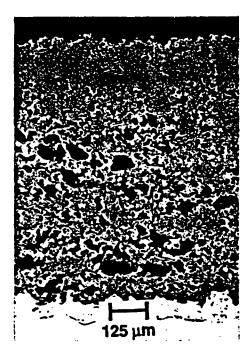


Fig.5 - Cross section of an as-deposited coating, showing typical microstructures of the porous and dense zirconia layers as well as the bond coat. Although these microstructures are representative, the zirconia layers in this photo are somewhat thicker than the corresponding layers of the actual prototype test platen and roll.

Therefore, test results discussed in the following sections of this paper are based on test hardware surfaced with the 5 - 7% porous zirconia top coat.

Laboratory Simulator Tests

The impulse drying performance of the plasma sprayed zirconia was initially tested by IPST using the same electro-hydraulic simulator (Fig. 1) that was used for the earlier monolithic metal and ceramic platen experiments. The performance of a 127 mm (5 in) diameter steel platen plasma sprayed with the multi-layer coating was compared to that of a comparable uncoated steel platen. The paper used for these experiments was a 205 g m⁻² single-ply linerboard, a heavy-weight paper grade that is highly susceptible to delamination. Linerboard handsheets were prepared and pre-steamed to a typical processing temperature of 358 K (85 °C) with 30% ingoing solids. Experiments were run at peak pressures of 3.1, 4.8, and 6.2 MPa (450, 695, and 900 psi) with initial platen temperatures ranging from 358 to 773 K (85 to 500 °C). A high-temperature polymer release agent, FreekoteTM 700 NC, was applied to both the steel and PSZ coated platens so that differences in release would not influence the results.

Water removal was quantified as a Moisture Ratio Change (MRC), defined as follows:

MRC = Ingoing Weight - Outgoing Weight Oven Dried Weight

It is apparent from this expression that a higher MRC value indicates better water removal. Impulse drying test results have shown that water removal increases as the platen is heated to higher temperatures before it is pressed against the test sheet [9, 10, 14]. However, the maximum initial temperature of the platen is limited by the onset of sheet delamination. In the laboratory simulator experiments, the onset of delamination with increasing initial platen temperature was determined by a careful visual examination and also by an out-of-plane ultrasonic test method. Table II compares the maximum temperature limits as determined by these two inspection methods and also shows the corresponding MRC values.

The results in Table II show that the performance of the plasma sprayed test platen is very similar to the uncoated steel platen at the lowest peak pressure, 3.1 MPa. However, the operating temperature limits for the coated platen at 4.8 and 6.2 MPa are roughly twice as high as those for the uncoated platen, resulting in a significant increase in water removal with the coated platen.

While water removal efficiency is important, enhanced sheet property development is also a major potential advantage of impulse drying. Once the operating temperature limits were defined, the platen materials were further compared in terms of maximum outgoing solids, sheet density, and specific elastic modulus. Fig. 6 shows a comparison of these results based on the most conservative temperature limits from Table II. Values for outgoing solids in Fig. 6 were computed as follows:

% Outgoing Solids = 100 x Oven Dried Weight Weight of Fiber + Weight of Water

Consistent with the MRC values in Table II, the results in Fig. 6 show little difference between the coated and uncoated platens at 3.1 MPa, but the coating afforded significant improvements in all of the measured properties at 4.8 and 6.2 MPa. The increased densities observed for the coated platen are consistent with the hypothesis that there was less flash vaporization deep within the sheet to cause fiber separation and a reduced density in the inner part of the sheet. The increased specific elastic modulus for the coated platen at 4.8 and 6.2 MPa further suggests a

Peak Pressure	Evaluation	Maximum Temp. (K)		Maximum MRC	
(MPa)	Method	Steel PSZ Coated		Steel PSZ Coated	
3.1	Visual	525	476	0.95	0.95
	Ultrasound	484	518	0.90	1.00
4.8	Visual	401	717	0.93	>1.20
	Ultrasound	350	717	0.88	>1.20
6.2	Visual	444	771	1.03	1.27
	Ultrasound	389	743	0.98	>1.25

Table II. Comparison of maximum initial platen temperature and moisture ratio change (MRC) for the bare steel test platen versus the partially stabilized zirconia (PSZ) coated test platen.

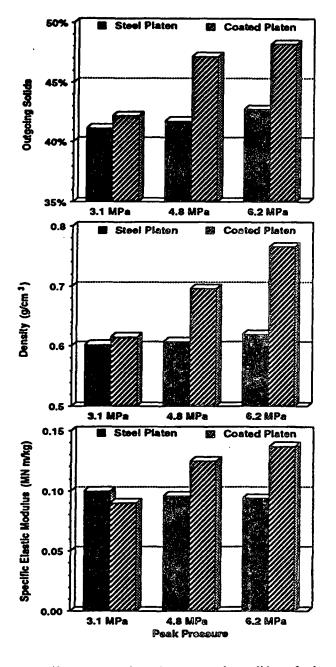


Fig. 6 - Comparison of maximum outgoing solids, soft platen density, and specific elastic modulus of impulse dried linerboard sheets in simulator tests with steel versus PSZ coated platens.

probable improvement in sheet strength, since the out-of-plane specific elastic modulus has been shown to be proportional to standard destructive strength tests [9].

Energy use calculations based on the platen test results also showed that impulse drying with the coated test platen was more energy efficient that conventional wet-pressing. For example, under conditions that would require 2257 kJ/kg for wet-pressing/evaporative drying, impulse drying with the ceramic coating requires only 666 kJ/kg, less than 1/3 of the energy consumed with the conventional drying process!

Evaluation of Coated Pilot-Scale Roll

Based on the encouraging results of the laboratory simulator tests, it was decided to test the prototype PSZ coating on an actual press roll. The objective was to determine whether a prototype ceramic-coated press roll could be used to impulse dry a heavyweight paper grade without inducing sheet delamination. A test roll was plasma sprayed with the same multi-layer coating that was used on the simulator platen. The coated roll was then diamond ground and installed on the first nip of a pilot-scale impulse dryer at IPST. As with the simulator test platens, FreekoteTM release agent was applied to the roll surface to inhibit adherence of the sheet to the roll. The roll surface was radiantly heated with infrared heaters, and an infrared pyrometer was used to monitor the temperature of the roll surface just before it entered the nip. The pyrometer output was tied to a controller that adjusted the heaters to maintain a constant ingoing surface temperature. The paper tested on the pilot impulse dryer was again a 205 g m⁻² linerboard made from an unbleached softwood kraft. In order to evaluate the potential benefits of impulse drying over single-felted wet pressing, drying experiments were conducted over a range of conditions, with ingoing roll surface temperatures of 373 to 703 K (100 to 430 °C), ingoing solids ranging from 30% to 45%, as well as 20 ms and 40 ms dwell times. The peak nip pressure was held constant at 6.2 MPa (900 psi), and the ingoing sheet temperature was held at 373 K (100 °C).

An extensive discussion of the results of all of these experiments may be found in [14]. To briefly summarize these results, it was found that impulse drying with the ceramic coated roll produced significant improvements in drying efficiency and also paper quality as compared to conventional wet-pressing technology. The best results were obtained with the longer, 40 ms, dwell time and an ingoing dryness of more than 40% solids. Under these conditions, the roll could be operated at surface temperatures of 644 K (371 °C) without sheet delamination, but evidence of delamination was observed at the next higher test temperature of 699 K (426 °C). With a 644 K (371 °C) ingoing roll surface temperature and an ingoing sheet dryness of 41% solids, an outgoing dryness of 60% solids was observed. This is a significant improvement over the 54% outgoing solids that can be achieved with conventional double-felted wet-pressing methods. Other properties, such as specific elastic modulus, burst index, and STFI strength indices, were also improved by impulse drying with the corranic-costed roll.

A comparison of results for comparable laboratory simulator and pilot roll experiments showed that the roll actually provided somewhat better water removal than the simulator. This slight additional improvement in performance is attributed to the fact that the simulator has no provision to automatically separate the waterlaten press felt from the sheet upon depressurization, whereas the felt and sheet are automatically separated as they leave the nip of the pilot impulse dryer.

Summary

Both laboratory simulator and pilot-scale roll press experiments have shown that the prototype plasma sprayed ceramic coating permits impulse drying of linerboard sheets at high surface temperatures without delamination. As a consequence, the amount of water removed by impulse drying was substantially more than can be removed by conventional methods. In addition, significant improvements were also observed in energy efficiency and in the physical properties of sheets impulse dried with the ceramic coating.

Additional testing is currently in progress to further optimize the design of the coating and the drying parameters. Further information about recent work on this development program may be found in [15-17]. A full-scale test of a plasma spray coated roll on a commercial paper machine is anticipated before the end of 1995.

References

- SPRAGUE, C.and H.P LAVERY, High-Intensity Drying Processes - Impulse Drying, Report 1 for Department of Energy Contract FG02-85CE40738, DOE/CE/40738-T1 (1985).
- LAVERY, H.P., High-Intensity Drying Processes Impulse Drying, Report 2 for Department of Energy Contract FG02-85CE40738, DOE/CE/40738-T2 (1987).
- LAVERY, H.P., High-Intensity Drying Processes Impulse Drying, Report 3 for Department of Energy Contract FG02-85CE40738, DOE/CE/40738-T3 (1988).
- ARENANDER, S. and D WAHREN, Impulse Drying Adds New Dimension to Water Removal, TAPPI Journal, 68-9 (1983).
- 5. BURTON, S., A Dynamic Simulation of Impulse Drying, A190 Project, The Institute of Paper Chemistry (1983).
- BURTON, S., Ph.D. Thesis, "An Investigation of Z-direction Density Profile Development During Impulse Drying," The Institute of Paper Chemistry (1986).
- CROUSE, J.W., Y.D. WOO, and C.H. SPRAGUE, Delamination: A Stumbling Block to Implementation of Impulse Drying Technology for Linerboard, TAPPI Engineering Conference, Atlanta, GA (1989).
- ORLOFF, D.L., High-Intensity Drying Processes Impulse Drying, Report 4 for Department of Energy Contract, FG02-85CE40738, DOE/CE/40738-T4 (1989).
- ORLOFF, D.I., High-Intensity Drying Processes Impulse Drying, Report 5 for Department of Energy Contract, FG02-85CE40738, DOE/CE/40738-T5 (1990).
- ORLOFF, D.L. Impulse Drying of Linerboard: Control of Delamination, 77th Annual Meet Can. Pulp and Paper Assoc., Montreal, Canada, Jan. 1991.
- Engineering Property Data On Selected Ceramics Volume III

 Single Oxides, Metals & Ceramics Information Center, BATTELLE Columbus Laboratory, MCIC-HB-07-Vol. III (1981).
- KUBEL, E.J. Jr., Powders Dictate Spray Coating Properties, Adv. Matl's & Proc., 138-6 Dec. (1990).

- SMITH, M.F., D.T. McGUFFIN, J.A. HENFLING, and W.J. LENLING, A Comparison of Techniques for the Metallographic Preparation of Thermal Sprayed Samples, Proc. 4th National Thermal Spray Conf., Pittsburgh, PA, May, 1991.
- ORLOFF, D.L., High-Intensity Drying Processes Impulse Drying, Report 6 for Department of Energy Contract, FG02-85CE40738, DOE/CE/40738-T6 (1991).
- 15 ORLOFF, D.L., and J.L. LINDSAY, The Influence of Yield, Refining and Ingoing Solids on the Impulse Drying Performance of a Ceramic Coated Press Roll, to be presented at TAPPI Papermakers Conf., Nashville, TN, Apr. 5-8, 1992.
- ORLOFF, D.L., and S.F. SOBCZYNSKI, Impulse Drying Pilot Press Demonstration: Ceramic Surfaces Inhibit Delamination, to be presented at SPCI-92, Belogna, Italy, May 19-20, 1992.
- ORLOFF, D.I., G. L. JONES, and P. M. PHELAN, The Effects of Heating Mode and Internal Roll Temperature on Roll Durability and Efficiency of Impulse Drying, to be presented at the Nat'l Heat Transfer Conf., San Diego, CA, Aug. 9-12, 1992.